

APPENDIX B
UV DISINFECTION SYSTEM DESIGN EXAMPLE

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Scheible⁽³⁰⁾ has presented a simplified design example to demonstrate how the model expression [5] can be used to design a new system.

STEP 1: WASTEWATER DATA COLLECTION.

- a. The treatment plant is a conventional activated sludge facility with the following design conditions:

$Q_{avg} = 1.9$ MGD (5000 l/min)
 $Q_{peak} = 3.8$ MGD (10000 l/min)
UV Transmittance, T_r , measured of 67%
Total Suspended Solids (TSS) = 20 mg/l
Initial Fecal Coliform $N_0 = 200,000/100$ ml
Disinfection Goal N , 200/100 ml from effluent permit.

- b. Calculate absorbance units per centimeter (A/cm)

$$\% \text{ Transmittance, } T_r, = 100 \times 10^{-(A/cm)}$$

$$67 = 100 \times 10^{-(A/cm)}$$

$$A/cm = 0.174$$

Calculate UV Coefficient of Absorption, α

$$\alpha = A \times 2.3 = 0.174 \times 2.3 = 0.4 \text{ cm}^{-1}$$

STEP 2: MODEL COEFFICIENT AND PARAMETERS.

From the literature $c = 0.26$, $m = 1.96$, $a = 1.45 \times 10^{-5}$ and $b = 1.3$

Therefore, for the example:

$$\begin{aligned} N_p &= c(TSS)^m \\ N_p &= 0.26(TSS)^{1.96} \end{aligned} \quad [6]$$

and

$$\begin{aligned} K &= a (I_{avg})^b \\ K &= 1.45 \times 10^{-5} (I_{avg})^{1.3} \end{aligned} \quad [7]$$

24 Aug 92

STEP 3: ESTABLISH REACTOR PARAMETERS AND EQUIPMENT CONDITIONS.

For illustrative purposes, the configuration chosen is a uniform array, with a centerline spacing, S , of 5.5 cm. The lamps will be G64T5 (Table 4-2), have an arc length, Z , of 1 x 47 cm, and a rated (nominal) UV output of 26.7 W at 253.7nm. Each lamp is sheathed in a quartz sleeve with diameter, d_q , of 2.3 cm. The dimensional layout of the array is depicted in Figure 4-15a, with the volume associated with each lamp/quartz included. In a uniform array, lamp spacing, $S=S_v=S_h$.

The average nominal intensity is presented on Figure 4-16 as a function of the UV coefficient of absorption. The lamps will be configured axially parallel to one another and the flow path perpendicular to the lamps. The values of the energy loss factors, F_p and F_l are set at 0.8 and 0.7, respectively as discussed in paragraph 3.3.1 step 3f. The maximum allowable headloss through the battery of lamps is set at 40 cm (16 in) and is exclusive of entrance and exit losses for the reactor.

STEP 4: DETERMINE REACTOR UV DENSITY

Compute Liquid Volume (Void Volume)

The liquid volume associated with each lamp/quartz is computed from:

$$\begin{aligned} V_v \text{ per lamp} &= (S^2 Z) - [\pi Z d_q^2 / 4] \\ V_v \text{ per lamp} &= [(5.5)^2 (147)] - [\pi (147) (2.3^2 / 4)] \\ V_v \text{ per lamp} &= 3840 \text{ cm}^3 \text{ (3.84 lit)} \end{aligned} \quad [10]$$

Compute UV Density, D

$$\begin{aligned} D &= \text{Total UV output/liq vol} \\ D &= \text{arc length} \times \text{UV output/liq vol} \\ D &= (26.7 \text{ w} / 3.84 \text{ liter}) \\ D &= 7 \text{ w/l} \end{aligned} \quad [9]$$

STEP 5: UV INTENSITY.

Determine Nominal Intensity

24 Aug 92

Enter Figure 4-16 (uniform array) with known values of $D = 7$ w/l and coefficient of absorption, α , $= 0.40 \text{ cm}^{-1}$ and read nominal I_{avg} of $17,500 \text{ } \mu\text{W}/\text{cm}^2$.

Adjust Intensity

$$\begin{aligned} I_{\text{avg}} &= \text{Nom } I_{\text{avg}} \times F_p \times F_t & [8] \\ I_{\text{avg}} &= 17,500 \times 0.8 \times 0.7 \\ I_{\text{avg}} &= 9,800 \text{ } \mu\text{W}/\text{cm}^2 \text{ (adjusted)} \end{aligned}$$

STEP 6: INACTIVATION RATE

$$\begin{aligned} K &= a (I_{\text{avg}})^b & [7] \\ K &= 1.45 \times 10^{-5} (9,800)^{1.3} \\ K &= 2.24/\text{sec} \end{aligned}$$

STEPS 7 and 8: SET HYDRAULIC LOADING RATE AND UV LOADING/PERFORMANCE

UV Loading Rate $= Q/W_n$ where Q = peak flow in lpm and W_n = nominal wattage. Once the loading is set, the nominal exposure time, t_n , is set using:

$$t_n = (V_v/W_n) / (Q/W_n) \quad [12]$$

For the example,

$$V_v/W_n = 1.144/W_n$$

and

$$t_n = (0.144/W_n) / (Q/W_n)$$

Calculate Dispersion in the Reactor

Set, dimensionless dispersion number, d_n , defined as $d_n = E/ux = 0.01$. Set $E = 15 \text{ cm}^2/\text{sec}$ which is similar to dispersion coefficients determined by test results. Thus ux must be greater than $15/0.01 \text{ cm}^2/\text{sec}$, and $u = 1500/x$.

Velocity $u = \text{UV exposure length}/\text{UV exposure time} =$

$$u = x/t_n$$

Expression for Effective Length of Reactor:

Substituting: $1500/x = x/t_n$

$$\text{and } x = (1500 t_n)^{1/2}$$

[15]

Table B-1 shows a summary of the calculations used to determine $\log (N'/N_0)$ for the configuration spacing, $S = 5.5$ cm. The $\log (N'/N_0)$ values are plotted in Figure B-1 as a function of the Q/W_n ratios. Note that the UV performance is based on the non-particulate effluent fecal coliform density. The particulate fecal coliform, density, N_p , would be additive.

Table B-1 Calculation of performance based on loading (uniform array, $S = 5.5$ cm)

Loading Q/W_n lpm/ W_n	Nominal ^a time, t_n (Sec)	Length ^b x (cm)	Velocity ^c u (cm/s)	$\log N'/N_0^d$ at K of $2.24s^{-1}$
0.5	17.2	160	9.3	-12.90
1.0	8.6	113	13.1	- 7.22
1.5	5.8	93	16.0	- 5.06
2.0	4.3	80	18.6	- 3.84
3.0	2.9	66	22.8	- 2.62
4.0	2.2	57	25.9	- 2.06
6.0	1.4	46	33.0	- 1.03

a $t_n = [0.144/W_n]/(Q/W_n)] \times 60 \text{ sec/min}$

b $x = (1500 t_n)^{1/2}$

c $u = x/t_n$

d $N'/N_0 = \exp \{ (ux/2E) \{ 1 - (1 + 4KE/u^2)^{1/2} \} \}$ for
 $E = 15 \text{ cm}^2/\text{sec}$ and $K = 2.24/\text{sec}$

STEP 9: ESTABLISH PERFORMANCE GOALS

Calculate Particulate Coliform Density (N_p)

For TSS = 20 mg/l (Step 1'), $c = 0.26$, and $m = 1.96$:

$$N_p = c(\text{TSS})^m$$

$$N_p = 0.26 (20)^{1.96}$$

$$N_p = 92/100 \text{ ml}$$

[6]

Calculate N' :

$$N' = (N - N_p)$$

[16]

24 Aug 92

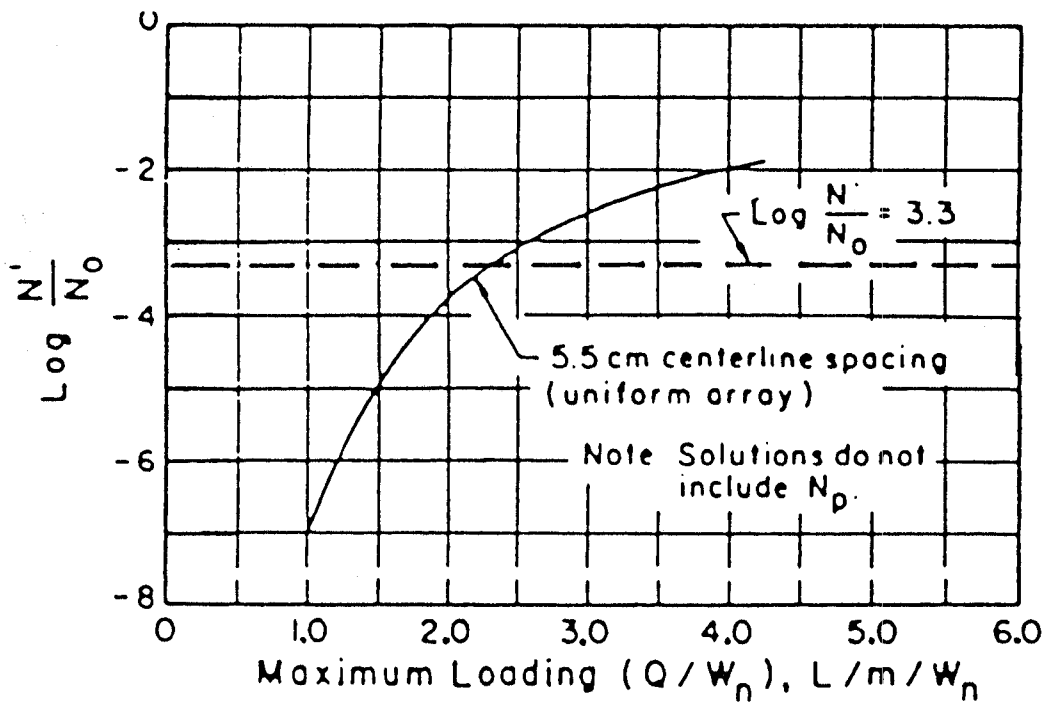


FIGURE B-1 Calculation of performance based on loading (uniform array, $s = 5.5$ cm) ⁽²⁸⁾

24 Aug 92

For the required effluent coliform limit, $N = 200/100$ ml
and $N_p = 92/100$ ml:

$$N' = 200 - 92 = 108/100 \text{ ml}$$

Calculate Required Performance

$$\text{Required performance} = \log (N'/N_0)$$

For $N_0 = 200,000/100$ ml (STEP 1)
and $N' = 108/100$ ml

$$\text{then, } \log (N'/N_0) = \log (108/200,000) = -3.3$$

STEP 10: SIZE REACTOR AND UV EQUIPMENT COMPONENTS

From Figure B-1, maximum Q/W_n allowed for $\log (N'/N_0)$ of -3.3 is 2.35 lpm per W_n , at the given intensity, in order to meet the 200/100 ml effluent coliform goal.

Calculate Equivalent Residence Time, t_n

$$t_n = (V_n/W_n) / (Q/W_n) \quad [12]$$

for $V_n/W_n = 0.144 \text{ l}/W_n$ (STEP 7)
and $Q/W_n = 2.35 \text{ lpm}/W_n$ (STEP 10),

then $t_n = (0.144 \text{ l}/W_n) / (2.35 \text{ lpm}/W_n)$
and $t_n = 0.0613 \text{ min} \times 60 \text{ sec/min} = 3.67 \text{ sec}$

Determine Number of Lamps

$$\text{No. Lamps} = [(Q)/(Q/W_n)] / \text{nominal watts per lamp} \quad [17]$$

for $Q = 10,000 \text{ lpm}$ (STEP 1)
 $(Q/W_n) = 2.35$ (STEP 10a)
watts/lamp = 26.7 (STEP 3)

$$\text{then number of lamps} = (10,000/2.35)/26.7 = 159$$

Compute Effective Length of Reactor

$$\text{Effective length, } x = (1500 t_n)^{1/2} \quad (\text{STEP 7}) \quad [15]$$

For $t_n = 3.67 \text{ sec}$ (STEP 10),

$$x = [(1500)(3.67)]^{1/2} = 74 \text{ cm}$$

Calculate No. of Lamps in x-direction

Lamps = $x/S = 74 \text{ cm}/5.5 \text{ cm} = 13.5$ since flow path is perpendicular to lamps

Summary

A total of 180 lamps is selected and placed in a 15 x 12 array. Recalculating, Q/W_n is now $10,000/(26.7 \times 180) = 2.08 \text{ lpm}$, $t_n = V_v/Q = 0.144/2.08 = 4.15 \text{ sec}$, $u = x/t_n = (5.5 \times 15)/4.15 = 19.8 \text{ cm/sec}$ and $d_n = E/ux = 15/(19.8)(5.5)(15) = 0.0091$. The example configuration is summarized in Table B-2.

Table B-2 Design sizing summary for 5.5 cm centerline spacing - uniform array

Length	15 lamps (66 cm)
Height	12 lamps (66 cm)
Total number of lamps	180
Q/W_n in lpm/ W_n	2.08
Exposure time, t_n (seconds)	4.15
Velocity, (cm/sec)	19.8
Dispersion No., d_n , at $E = 15 \text{ cm}^3/\text{sec}$	0.0092
Total power (KW)	14.4

The Q/W_n is now 2.08, which is below the maximum allowable of 2.35 (STEP 10). The dispersion number, dn , is slightly less than the objective of 0.01 (STEP 7).

Calculate Head Loss

$$h_L = c_f (x) (u^3) \quad [18]$$

where $c_f = 0.00025 \text{ sec}^2/\text{cm}^2 \text{ }^{(31)}$
 $x = 5.5 \times 15 = 82.5 \text{ cm}$
 $u = 19.8 \text{ cm}^2$

$$h_L = (0.00025)(82.5)(19.8)^2 = 8.0 \text{ cm} < 40 \text{ cm}$$

(o.k.)

The example is meant to illustrate the use of the mathematical modeling approach for a UV process design. The appropriate calibration data must first be obtained for the site specific wastewater application. The calculations are

24 Aug '92

only an example and should not be used in the design of a system. Reference 27, Chapter 7 contains a more thorough computational analysis procedure and example problem.